IN THE CLAIMS:

1. – 2. (Cancelled).

3. (Previously Presented): The process according to Claim 15 wherein the regeneration gas passes through a catalyst bed of the second coke-burning zone in a centrifugal or centripetal radial direction and then passes through a catalyst bed of the first coke-burning zone in a centrifugal or centripetal radial direction.

4. (Previously Presented): The process according to Claim 15 wherein the regeneration gas passes through a catalyst bed of the second coke-burning zone in a centrifugal radial direction and then passes through a catalyst bed of the first coke-burning zone in a centrifugal radial direction.

5. (Previously Presented): The process according to Claim 15 wherein the operating pressure of the regeneration process is in the range of 0.3 - 0.9 MPa.

6. (Cancelled).

7. (Previously Presented): The process according to Claim 15 wherein the regeneration gas at the inlets of the first and second coke-burning zones has an oxygen concentration in the range of 0.2-1.0 v%.

8. (Previously Presented): The process according to Claim 15 wherein the regeneration gas entering the first-coke burning zone is at a temperature in the range of 410 - 480°C.

9. (Previously Presented): The process according to Claim 15 wherein the regeneration gas entering the second coke-burning zone is at a temperature in the range of 480 - 520°C.

10. (Cancelled).

11. (Previously Presented): The process according to Claim 15 or 17 wherein said inner screen of the first coke-burning zone is a cylinder with a uniform diameter, or a tapered cylinder with a downwardly reduced diameter.

12. (Previously Presented): The process according to claim 11, wherein the diameter of said inner screen is linearly reduced from its top wherein its minimal diameter is 60 - 90% of its maximal diameter.

13. (Previously Presented): The process according to claim 11, wherein the diameter of said inner screen is reduced at a point 40 - 60% from the top of the height of the first coke-burning zone in a straight down manner so that the diameter at the bottom of said inner screen is 60 - 90% of the diameter at the top of said inner screen.

14. (Previously Presented): The process according to Claim 15 or 17 wherein said inner screen of the second coke-burning zone is cylindrically shaped.

15. (Currently Amended): A process of continuously regenerating ~~catalysts~~ catalyst particles comprising passing deactivated catalyst particles downwardly, in sequence, through a first coke-burning zone, said first coke-burning zone comprising a radial bed, an inner screen and an outer screen; a second coke-burning zone, said second coke-burning zone comprising a radial bed, an inner screen and an outer screen; an oxychlorination zone and a calcination zone, wherein said deactivated catalysts particles are contacted in said first coke-burning zone with regeneration gas from said second coke-burning zone, supplementary dry air and an inert gas; said regeneration gas being withdrawn from said first coke-burning zone and recycled back into said second coke-burning zone where it is contacted with said catalyst particles previously contacted in said first coke-burning zone, said regeneration gas having a water concentration of 10 to 200 ppmv.

16. (Previously Presented): The process according to Claim 15 wherein said regeneration gas is dried after being withdrawn from said first coke-burning zone before being recycled into said second coke-burning zone.

17. (Currently Amended): A process of continuously regenerating catalyst particles comprising passing deactivated catalyst particles from moving bed reactors downwardly by gravity, in sequence, through a first coke-burning zone, said first coke-burning zone comprising a radial bed, an inner screen and an outer screen; a second coke-burning zone, said second coke-burning zone comprising a radial bed, an inner screen and an outer screen; an oxychlorination zone; and a calcination zone wherein a dry oxygen-containing gas at a

temperature in the range of between 480°C and 520°C is introduced into the bottom of said second coke-burning zone; passing said gas through a catalyst bed of said second coke-burning zone in a centrifugal or centripetal radial direction wherein coke present on said catalyst particles is ~~are~~ burned off; cooling said gas from said second coke-burning zone to a temperature in the range of 410°C to 480°C by adding dry air and a dry inert gas; introducing said gas, passed through said second coke-burning zone, into said first coke-burning zone; passing said gas through a catalyst bed of said first coke-burning zone in a centrifugal or centripetal radial direction wherein coke is burned off said catalyst particles; withdrawing said gas from said first coke-burning zone; mixing said withdrawn gas with outlet gas from said oxychlorination zone; drying said gas in a recovery system wherein said gas is dried; passing said dry gas through a compressor; heating said compressed dry gas to a temperature in a range of 480°C to 520°C; and recycling said heated compressed dry gas to said second coke-burning zone wherein said recycled gas enters said first and said second coke-burning ~~zone~~ zones having an oxygen concentration in a range of 0.2 to 1.0 v%; and wherein said recycled gas enters said second coke-burning zone having a water concentration of 10 to 200 ppmv, said process occurring at an operating pressure in the range of 0.3 MPa to 0.9 MPa.